

# Challenges in Developing High Drug Loaded Redispersible Amorphous Nanoparticle Formulations of BCS IV Compound

23<sup>rd</sup> Jan 2025, SCPDG

Mengqi (Miki) Yu, Devalina Law

AbbVie, North Chicago IL

Journal of Pharmaceutical Sciences 113 (2024) 1007–1019

Contents lists available at ScienceDirect

 **Journal of Pharmaceutical Sciences**

journal homepage: [www.jpharmsci.org](http://www.jpharmsci.org)

Pharmaceutics, Drug Delivery and Pharmaceutical Technology

**Proof-of-Concept in Developing a 45% Drug Loaded Amorphous Nanoparticle Formulation** 

Hitesh S. Purohit<sup>a,\*</sup>, Deliang Zhou<sup>b</sup>, Mengqi Yu<sup>a</sup>, Maryam Zaroudi<sup>c</sup>, Hardeep Oberoi<sup>d</sup>, Angélica de L.Rodríguez López<sup>d</sup>, Manish S. Kelkar<sup>e</sup>, Yan He<sup>f</sup>, Bradley Gates<sup>g</sup>, Nandkishor Nere<sup>e</sup>, Devalina Law<sup>h,\*</sup>

Purohit et al. JPS 113(2024) 1007-1019

Contents lists available at ScienceDirect

 **Journal of Pharmaceutical Sciences**

journal homepage: [www.jpharmsci.org](http://www.jpharmsci.org)

Pharmaceutics, Drug Delivery and Pharmaceutical Technology

**Scale-up and clinical bioavailability assessment of a 45 % drug loaded amorphous nanoparticle formulation of a BCS IV compound for oral delivery**

Mengqi Yu<sup>a</sup>, Deliang Zhou<sup>a,1</sup>, Hardeep S. Oberoi<sup>d</sup>, Ahmed Hamed Salem<sup>b,c</sup>, Laura A. McKee<sup>d,2</sup>, Jason R. Arnholt<sup>e</sup>, Hitesh S. Purohit<sup>a,\*</sup>, Devalina Law<sup>a,\*</sup>

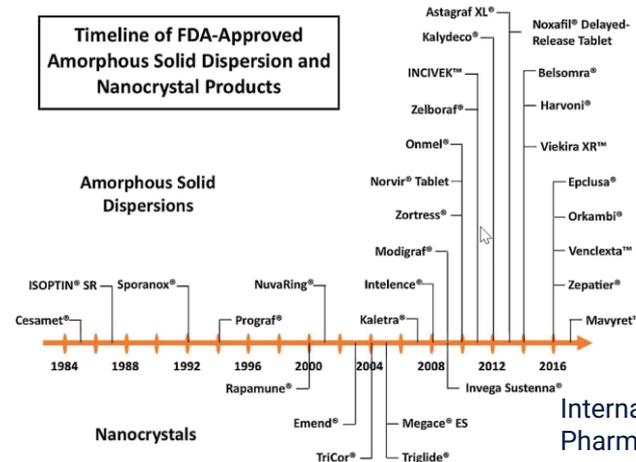
Yu et al. JPS 114(2025) 383-393

# Trend of solubilization challenge for NCE

- There is a growing trend for small molecules that fall in the “poorly soluble/insoluble” category
- About 40% of Marketed products are BCS II/IV and projected to increase to 80%+
- In the last 20 years increasing number of drug products using Amorphous Solid Dispersion (ASD) technology have been approved by FDA

Class I	High solubility, high permeability Marketed 35% - Candidates 5-10%
Class II	Low solubility, high permeability Marketed 30% - Candidates 60-70%
Class III	High solubility, low permeability Marketed 25% - Candidates 5-10%
Class IV	Low solubility, low permeability Marketed 10% - Candidates 10-20%

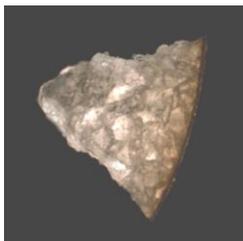
Pharmaceutics 2017, 9, 50



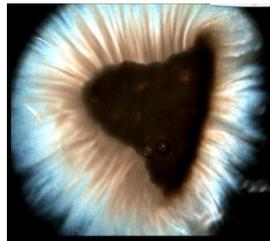
International Journal of  
Pharmaceutics 535 (2018) 379

# Why Amorphous Nanoparticles?

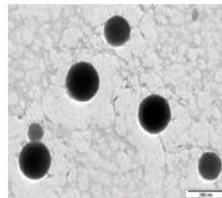
- What's happening during dissolution of ASD?
  - Supersaturation → liquid-liquid phase separation (LLPS) or glass-liquid phase separation (GLPS) → drug rich nanoparticles



ASD particle  
25 X magnification



LLPS formation in  
aqueous media

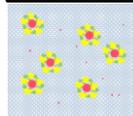


Cryo - TEM  
Drug rich  
nanoparticles

Opportunity: directly engineer nanoparticles

- Similar bioavailability to ASD
- Higher drug load

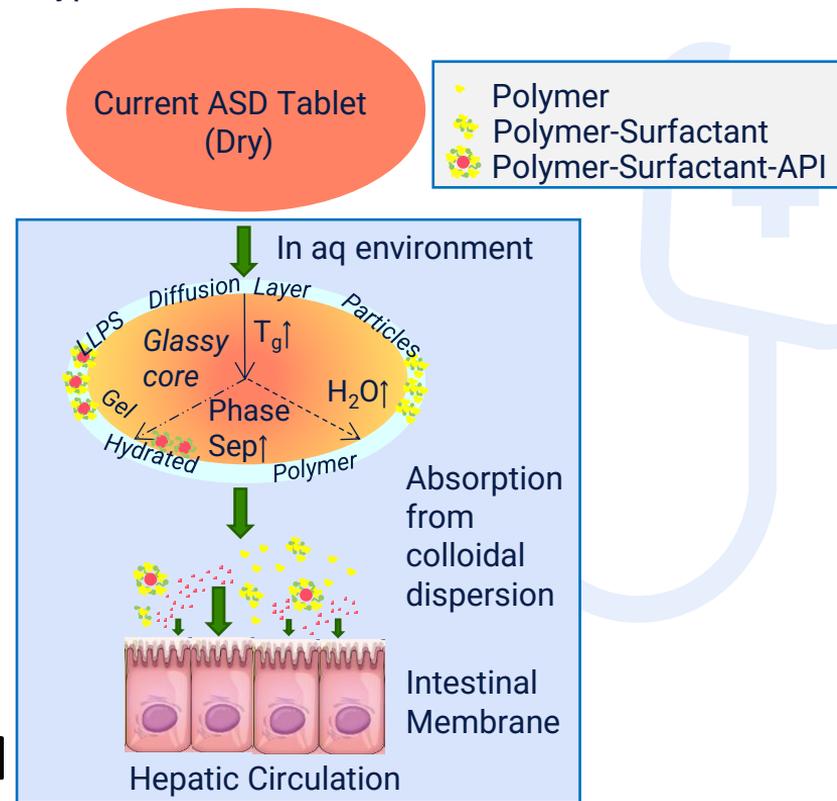
Delivered



What if eliminated?



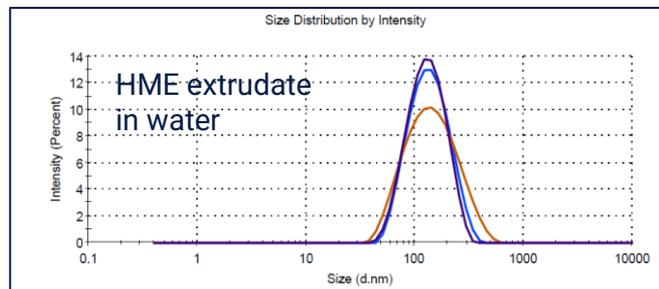
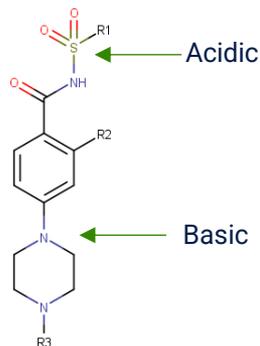
## Hypothesis : Release Mechanism



# Directly Engineered Nanoparticles: from Bench to Pilot Plant

## Model compound Compound X

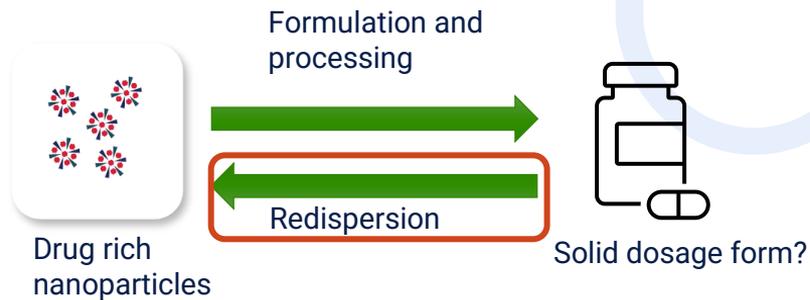
BCS IV Compound  
Zwitterionic @ pH 6.8  
Solid forms: numerous  
HME extrudates ~10% API



Particle size distribution by dynamic light scattering

## Challenges

1. How to generate amorphous nanoparticles (ANP)?
2. How to maintain stability of ANPs?
3. Can these ANPs be processed into a solid dosage form?
4. Can the dosage forms redisperse back to nanoparticles during dissolution?
5. How to scale it up?
6. Would this concept work (clinical performance)?

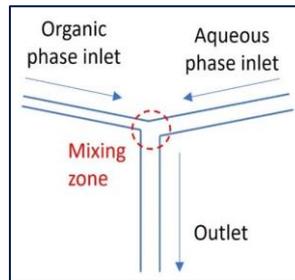


# Generating amorphous nanoparticles by solvent anti-solvent precipitation

## Solvent anti-solvent precipitation using impinging jet

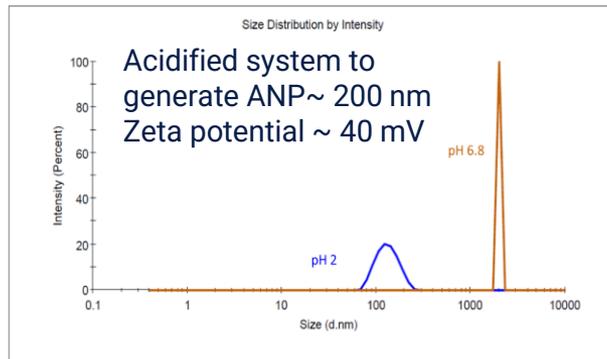
- Supersaturation and mixing at impinging site generated drug rich nanoparticles
- THF selected to solubilize Compound X in organic phase (due to solvate in other solvents)
- Acidified system (API ionized) enabled ANP generation (~200nm) and surface charge
- ANP size was optimized by changing ratio, flow rates, composition

Organic phase	
THF	95%
1M HCl	5%
Compound X	58.5 mg/mL



Aqueous phase	
0.01 N HCl	100%
PVPVA	0.27 mg/mL
Tween 80	0.27 mg/mL

Dilute nanoparticle suspension  
API/PVPVA/Tween 80 - 90/5/5  
Solid load in suspension ~ 0.5% w/v

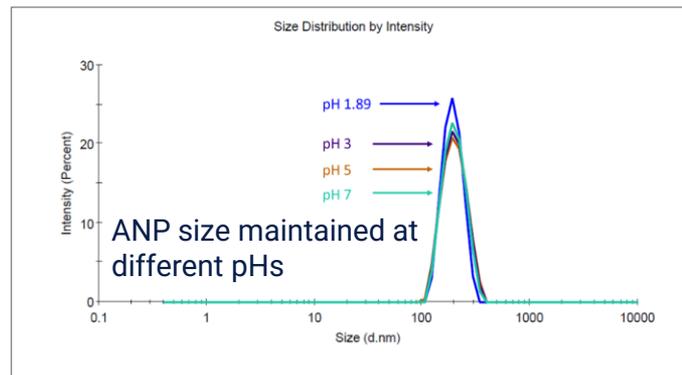


Organic to aqueous ratio	Size (nm)	PDI	Z potential (mV)
1: 6	390	0.029	42.1 ± 6.20
1: 9	180	0.032	43.2 ± 6.00
1: 12	111	0.076	38.2 ± 6.75
1: 14	130	0.110	36.6 ± 6.07

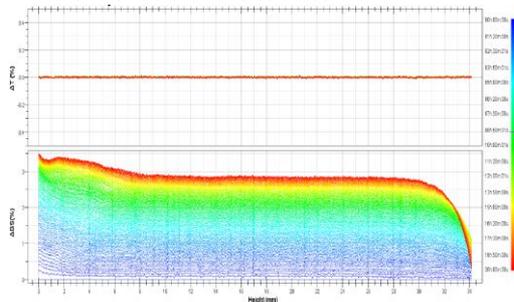
# Generating amorphous nanoparticles by solvent anti-solvent precipitation

## Stability of ANP in suspension

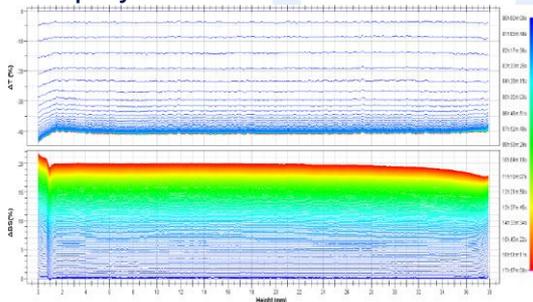
- Acidified system imparts surface charge to stabilize ANPs
- ANP maintained stability after generation when bulk pH was changed to 3, 5, and 7.
- Turbiscan (light scattering index) demonstrates no sedimentation within 20 hrs after generation using polymer and surfactant



Stable for 20 hrs with 5% PVPVA 5% Tween 80



Rapid sedimentation without polymer & surfactant



# Removal of organic solvent and stabilization of ANP for drying

## Solvent removal, washing and up-concentration was performed by tangential flow filtration (TFF)

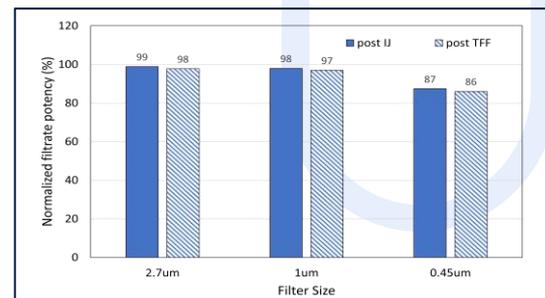
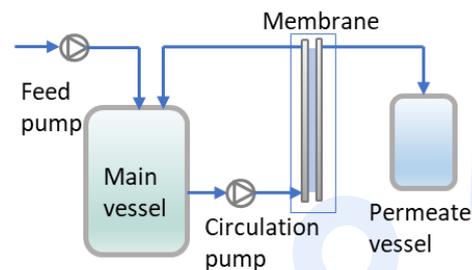
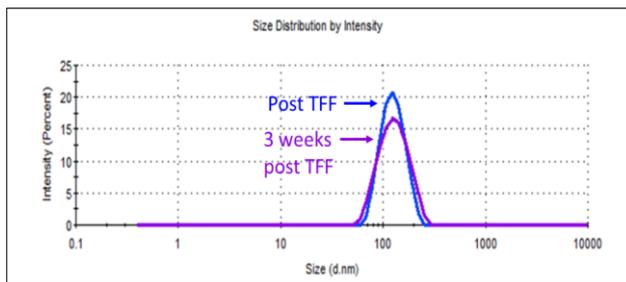
- THF level dropped to 0.13%/almost 100% removed  
pH  $\geq$  3
- Wet  $T_g$  (two  $T_g$ ) values even in the presence of THF
- These nanoparticles have been shown to exhibit core-shell structures
- Low  $T_g$  requires stabilization poses challenges for drying

## ANP Suspension of Compound X

- Suspension had 15% solid content
- 97% were below 1 micron in size
- 86% below 450 nm
- Stable for at least 3 weeks

Wet  $T_g$  of the ANPs in the presence and absence of THF

Sample	$T_g^1$ (°C)	$T_g^2$ (°C)
Post IJ (THF-water)	48	63
Post TFF (water)	46	79



Filtrate potency data for the nanosuspension before and after TFF

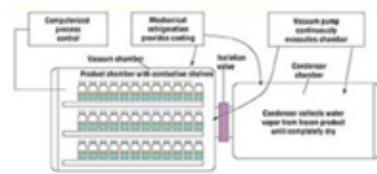
# From suspension to solid dosage form

## Freeze drying of the 15% solid containing suspension into solid powder with addition of sugar

- Sucrose and Trehalose containing formulations produced
- Cakes have porous structures
- Matrix exhibited embedded nanoparticles
- Added to water resulted in ANP suspension
- ~ 80% of the particles was below 450nm
- Visually trehalose cake re-dispersed faster

## ANP Formulation Selected for in vivo studies

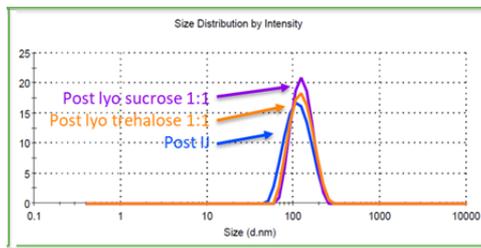
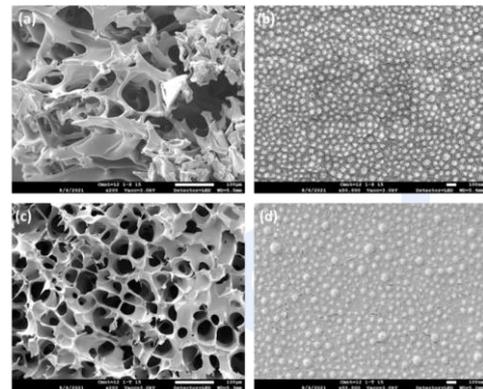
Composition	Function	[%]
Compound X	Active	45
Copovidone	Polymer	2.5
Polysorbate 80	Surfactant	2.5
Trehalose	drying-protectant	50
<b>Total</b>		<b>100</b>



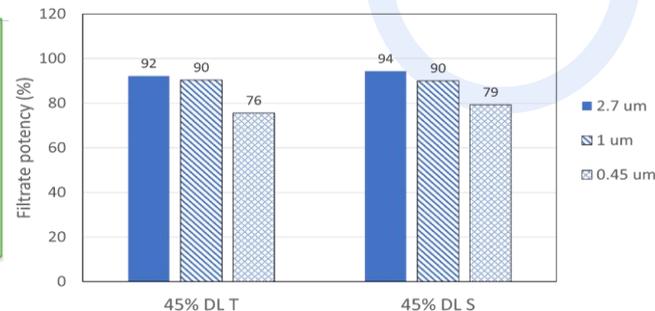
Freeze drying

	Sugar	Tot. solid load (%)	ANP/sugar ratio	Final DL(%)
1	Sucrose	15	1:1	45
2	Trehalose	15	1:1	45
3	Mannitol	15	1:1	45
Control	-	15	No sugar	90

Structure of FD cake: top trehalose; bottom sucrose



Dispersibility by DLS



# Scale up & In vivo studies in dogs

## Scale-Up Surprises

- Filter Potency revealed loss of dispersibility: 50% compared to 80% below 450nm
- qNMR studies revealed that the polymer was being lost during TFF
- Screening studies performed with post TFF polymer addition
- 2-8% Polymer when added post TFF exhibited comparable re-dispersion

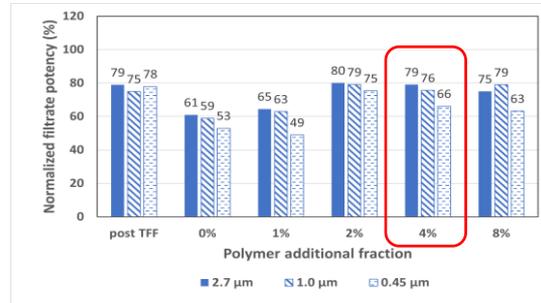
## Final formulation

- 45% Compound X
- Trehalose needed to be slightly reduced

## Fed and Fasted Studies in Dogs

- Results compare with ASD tablets  
Comparable in fasted state  
Lower exposure (60% AUC) in fed state
- With food HME tablets exhibited 4.6 times increase in AUC while ANP was 1.6 times probably because the tablets were retained in the stomach in the presence of food

Filtrate potency of larger batches after freeze drying



45% Drug Loaded ANP Formulation

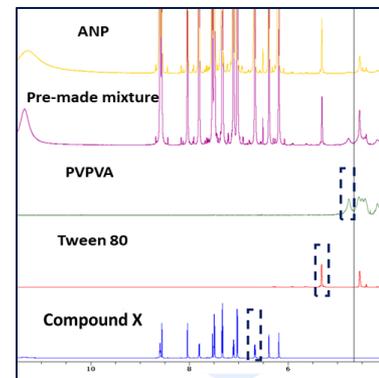
Component	Percent (w/w)
Compound X	45
PVPVA	4.5
Tween 80	2.5
Trehalose	48

Fasted State Dog Study

	$t_{1/2}$	$C_{max}$	$T_{max}$	$AUC_{inf}$	Point Estimates	
					$C_{max}$	AUC
Tablet	17.1	2.52 (0.43)	4.2 (0.4)	52.4 (7.2)		
ANP Suspension	16.0	2.65 (0.55)	3.8 (0.5)	51.8 (9.2)	0.997	0.967

Fed State Dog Study

	$t_{1/2}$	$C_{max}$	$T_{max}$	$AUC_{inf}$	Pt. Estimate	
					$C_{max}$	AUC
Tablet: reference	21.0	12.5 (1.55)	3.0 (0.8)	241 (19.6)		
ANP Suspension	17.2	6.64 (1.50)	3.4 (0.7)	167 (48.3)	0.48	0.60



1D proton spectral overlay for samples (from bottom to top) of Compound X, Tween-80, copovidone (PVPVA), pre-made mixture, and ANP. The highlighted proton signals were selected for building the standard curve

$t_{1/2}$  [hr; harmonic mean];  $C_{max}$  [ $\mu\text{g}/\text{mL}$ ];  $T_{max}$  [hr]; AUC [ $\mu\text{g}\cdot\text{hr}/\text{mL}$ ]

# Scale up challenges – pilot scale

## Preparation steps

ANP generation  
by impinging jet



Solvent removal  
by TFF



Obtain solid form  
by freeze drying

Continuous process can be scaled by longer run time

Semi continuous process can be scaled by longer run time

Freeze drying can be scaled by a larger batch size

New solid form occurred during engineering run

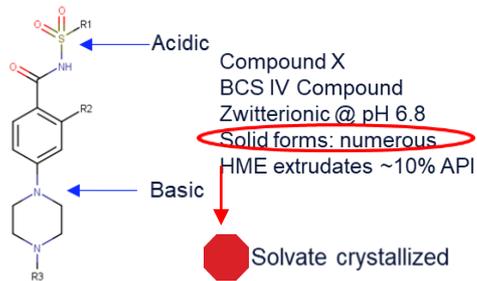
Are ANPs stable during the longer run?

Polymer loss during TFF resulted in decrease in redispersibility

# Challenges in scale up – generation of a large batch of ANP

## Scale-Up Surprises

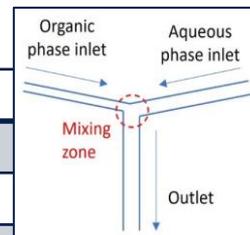
- A THF solvate of HCl salt precipitated
- Concentration of API in the Organic was decreased by 2.5x
  - Concentration of organic in suspension increased
  - Batch size changed from 60L to 140L, longer processing time posed stability concerns
  - Rapid particle size increase during engineering run
  - ANP suspension was chilled after generation
  - Lab batch PSD determined by DLS was 141 nm but the cold collection dropped the clinical batch PSD to 75 nm



Removal of organic solvent was critical for suspension stability and redispersibility

Organic phase	
THF	95%
1M HCl	5%
Compound X	58.5 mg/mL

Dilute nanoparticle suspension  
API/PVPVA/Tween 80 - 90/5/5  
Solid load in suspension ~ 0.2% w/v

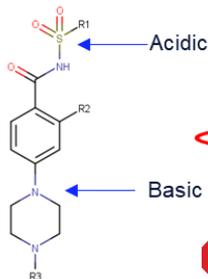


23.4 mg/mL

# Challenges in scale up – generation of a large batch of ANP

## Scale-Up Surprises

- A THF solvent of HCl salt precipitated
- Concentration of API in the Organic was decreased by 2.5x
  - Concentration of THF in ANP suspension increased
  - Batch size changed from 60L to 140L, longer processing time posed stability concerns
  - Rapid particle size increase during engineering run
- ANP suspension was chilled after generation
- Lab batch PSD determined by DLS was 141 nm but the cold collection dropped the clinical batch PSD to 75 nm



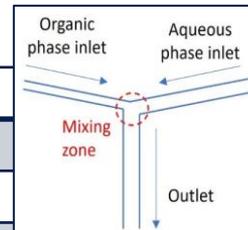
Compound X  
BCS IV Compound  
Zwitterionic @ pH 6.8  
**Solid forms: numerous**  
HME extrudates ~10% API

Basic  
Solvate crystallized

Removal of organic solvent was critical for suspension stability and redispersibility

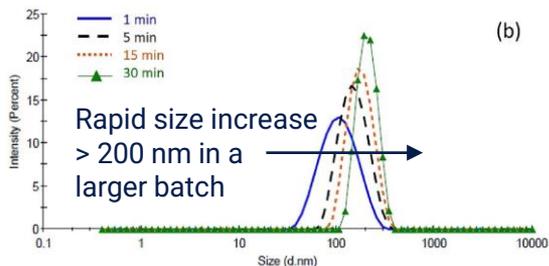
### Organic phase

THF	95%
1M HCl	5%
Compound X	58.5 mg/mL



23.4 mg/mL

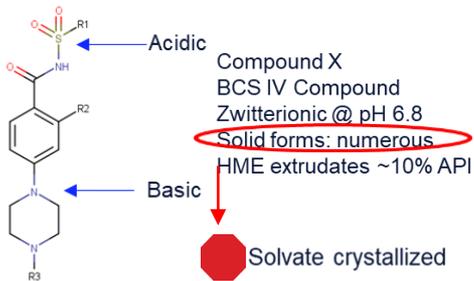
Dilute nanoparticle suspension  
API/PVPVA/Tween 80 - 90/5/5  
Solid load in suspension ~ 0.2% w/v



# Challenges in scale up – generation of a large batch of ANP

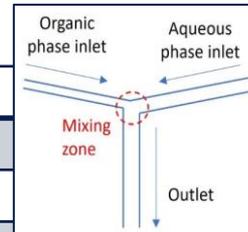
## Scale-Up Surprises

- A THF solvate of HCl salt precipitated
- Concentration of API in the Organic was decreased by 2.5x
  - Concentration of THF in ANP suspension increased
  - Batch size changed from 60L to 140L, longer processing time posed stability concerns
  - Rapid particle size increase during engineering run
- ANP suspension was chilled after generation
- Lab batch PSD determined by DLS was 141 nm but the cold collection dropped the clinical batch PSD to 75 nm



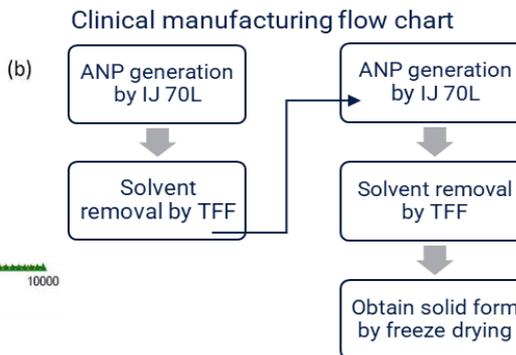
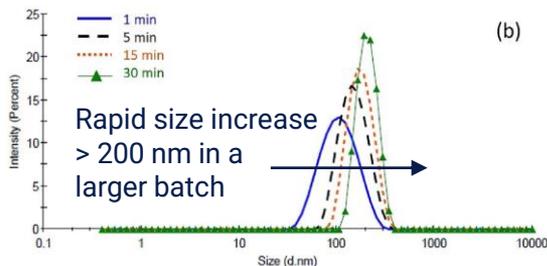
Removal of organic solvent was critical for suspension stability and redispersibility

Organic phase	
THF	95%
1M HCl	5%
Compound X	58.5 mg/mL



23.4 mg/mL

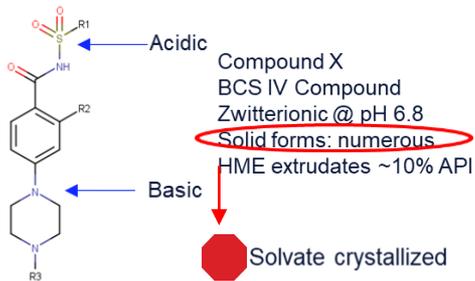
Dilute nanoparticle suspension  
API/PVPVA/Tween 80 - 90/5/5  
Solid load in suspension ~ 0.2% w/v



# Challenges in scale up – generation of a large batch of ANP

## Scale-Up Surprises

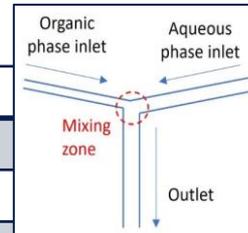
- A THF solvate of HCl salt precipitated
- Concentration of API in the Organic was decreased by 2.5x
  - Concentration of THF in ANP suspension increased
  - Batch size changed from 60L to 140L, longer processing time posed stability concerns
  - Rapid particle size increase during engineering run
- ANP suspension was chilled after generation
- Lab batch PSD determined by DLS was 141 nm but the cold collection dropped the clinical batch PSD to 75 nm



Removal of organic solvent was critical for suspension stability and redispersibility

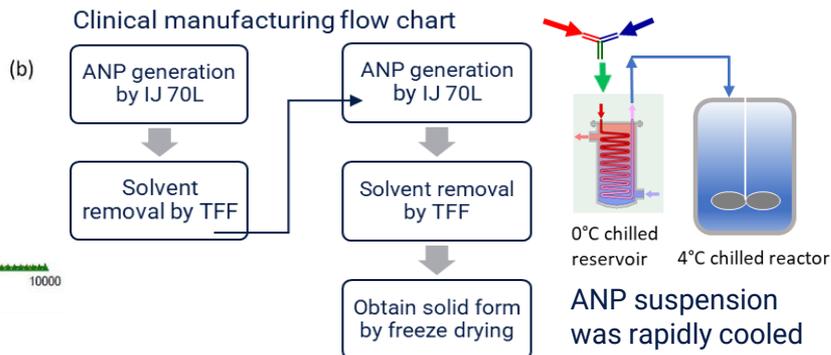
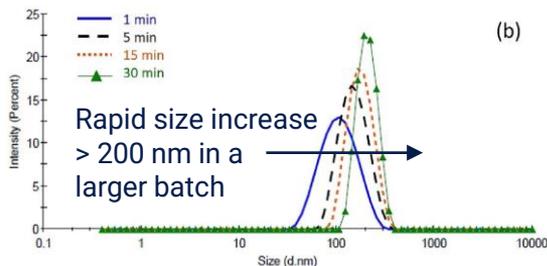
### Organic phase

THF	95%
1M HCl	5%
Compound X	58.5 mg/mL



23.4 mg/mL

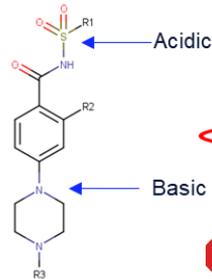
Dilute nanoparticle suspension  
API/PVPVA/Tween 80 - 90/5/5  
Solid load in suspension ~ 0.2% w/v



# Challenges in scale up – generation of a large batch of ANP

## Scale-Up Surprises

- A THF solvate of HCl salt precipitated
- Concentration of API in the Organic was decreased by 2.5x
  - Concentration of THF in ANP suspension increased
  - Batch size changed from 60L to 140L, longer processing time posed stability concerns
  - Rapid particle size increase during engineering run
- ANP suspension was chilled after generation
- Lab batch PSD determined by DLS was 141 nm but the cold collection dropped the clinical batch PSD to 75 nm

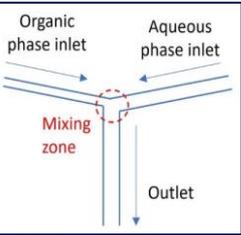


Compound X  
BCS IV Compound  
Zwitterionic @ pH 6.8  
**Solid forms: numerous**  
HME extrudates ~10% API

**Solvate crystallized**

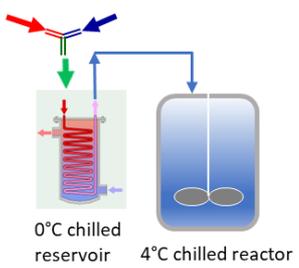
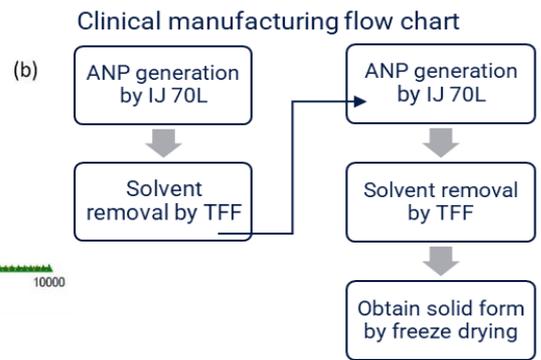
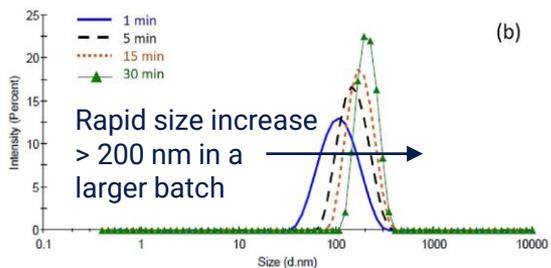
Removal of organic solvent was critical for suspension stability and redispersibility

Organic phase	
THF	95%
1M HCl	5%
Compound X	58.5 mg/mL

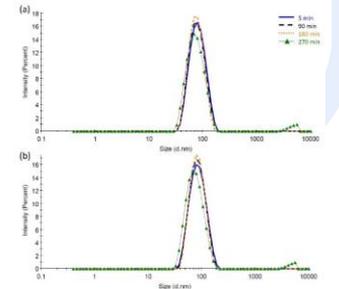


23.4 mg/mL

Dilute nanoparticle suspension  
API/PVPVA/Tween 80 - 90/5/5  
Solid load in suspension ~ 0.2% w/v



ANP suspension was rapidly cooled



Both batches produced ANP of 75 nm

# Challenges in obtaining redispersible solid dosage form

## Freeze drying of 45% DL suspension into solid powder

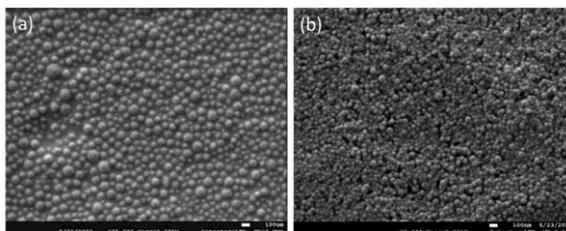
- ANP size of clinical batch smaller than laboratory batch 75 nm vs 140 nm
- Redispersion of clinical batch lower than laboratory

Clinical: ~ 65% smaller than 450 nm  
 Lab: ~90% smaller than 450 nm  
 Likely due to smaller particles and larger surface area

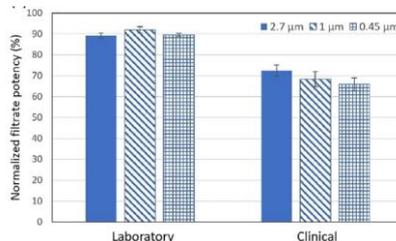
- FD powder for oral suspension as final dosage form

%(w/w)	Compound X	PVPVA	Tween 80
Composition	95.20	1.27	3.53
% RSD <sup>a</sup>	0.15	7.23	1.66

## Composition by NMR after TFF



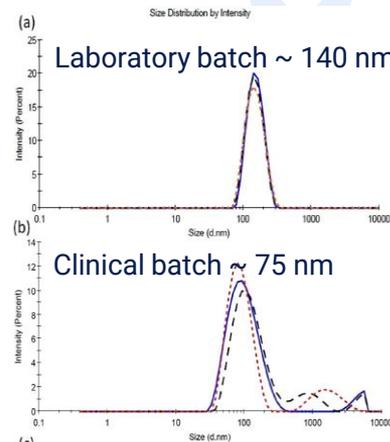
Laboratory batch ANP size > clinical batch



Redispersibility lab scale > clinical scale

%(w/w)	Theoretical	Actual
Compound X	45.0	45.3
PVPVA	2.5	2.6
Tween 80	2.5	1.7
Trehalose	50.0	50.4
Total	100.0	100.0

## Compounding before freeze drying



# Proof of concept of ANP dosage form of 45% DL

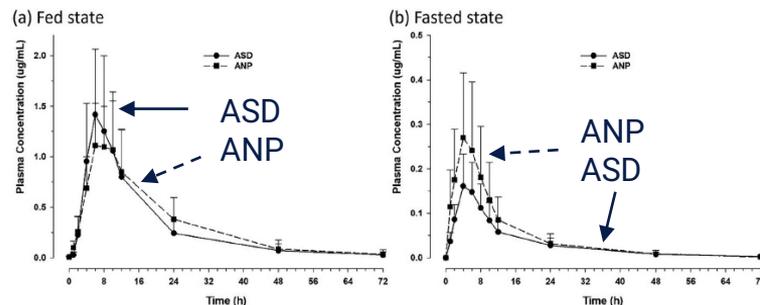
TFF Suspension was FD after polymer and trehalose incorporation

Dosed to humans as reconstituted suspension

Under **fed** condition, ANP formulation was close to meeting BE for AUC and had 21% lower  $C_{max}$ , compared to ASD tablets

Under **fasted** condition, ANP formulation showed enhanced bioavailability and lower food effect compared to ASD tablets

Proof of concept that directly engineered ANP has comparable bioavailability while maintaining a high drug load at 45% DL (vs 10% ASD tablets)



Pharmacokinetic Parameters (units)	ASD Tablets	ANP Formulation
<b>Fed (Cohort 1, N = 12)</b>		
$C_{max}$ ( $\mu\text{g}/\text{mL}$ )	1.54 (1.65, 41)	1.22 (1.31, 35)
$T_{max}^a$ (h)	6.0 (4.0 – 12.0)	8.0 (6.0 – 12.0)
$t_{1/2}^b$ (h)	13.6 (3.32)	11.9 (2.73)
$AUC_t$ ( $\mu\text{g}\cdot\text{h}/\text{mL}$ )	19.8 (21.8, 50)	22.2 (23.8, 42)
$AUC_\infty$ ( $\mu\text{g}\cdot\text{h}/\text{mL}$ )	20.4(22.5, 53)	22.8 (24.6, 46)
<b>Fasting (Cohort 2, N = 12)</b>		
$C_{max}$ ( $\mu\text{g}/\text{mL}$ )	0.147 (0.162, 44)	0.243 (0.286, 56) <sup>c</sup>
$T_{max}^a$ (h)	4.0 (4.0 – 8.0)	4.0 (4.0 – 6.0) <sup>c</sup>
$t_{1/2}^b$ (h)	12.9 (2.87)	11.7 (3.63) <sup>c</sup>
$AUC_t$ ( $\mu\text{g}\cdot\text{h}/\text{mL}$ )	2.07 (2.28, 48)	2.91 (3.40, 60) <sup>c</sup>
$AUC_\infty$ ( $\mu\text{g}\cdot\text{h}/\text{mL}$ )	2.14 (2.37, 48)	3.02 (3.50, 59) <sup>c</sup>

# Summary

**Directly engineered ANP at 45% DL was developed for BCS IV compound from lab to pilot scale**

**ANP formulation had comparable bioavailability as HME tablets at 10% DL with a lower food effect**

Challenges	Mitigation
Generation of IJ by solvent and anti-solvent precipitation	Screened solvent, polymer, surfactant as well as pH adjustment; Optimized IJ process parameters
Stability of ANP after generation	Understanding stabilization mechanism and design organic solvent removal
New solid form occurred during scale up	Lowered concentration of Compound X in solution
Stability of ANP at a larger scale	Control particle size increase by controlling temperature of generated ANP and reducing processing time
Ensure redispersibility after drying	Screened different sugars and identified trehalose

# Acknowledgement

## **NCE Formulations**

Hardeep Oberoi

Hitesh Purohit

Hong Yong

Craig Fowler

Deliang Zhou

Maryam Zaroudi

## **NBE**

Angelica Rodriguez Lopez

Tong Zhu

Ehab Moussa

## **PRD / S&T**

Nandkishor Nere

Manish Kelkar

Bradley Gates

Theodore Tharp

Laura McKee

Christopher Vitale

## **Analytical**

John Roth

Victoria Zalizna

Jessica Hoskins

Jason Arnholt

Adam Zaczek

Yan He

abbvie

# ANP formulation stability

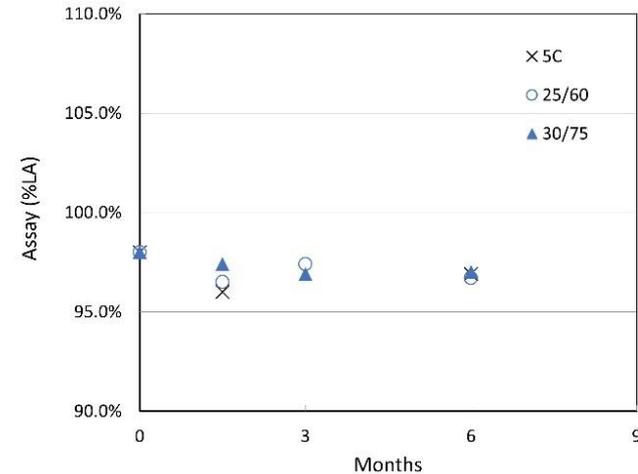
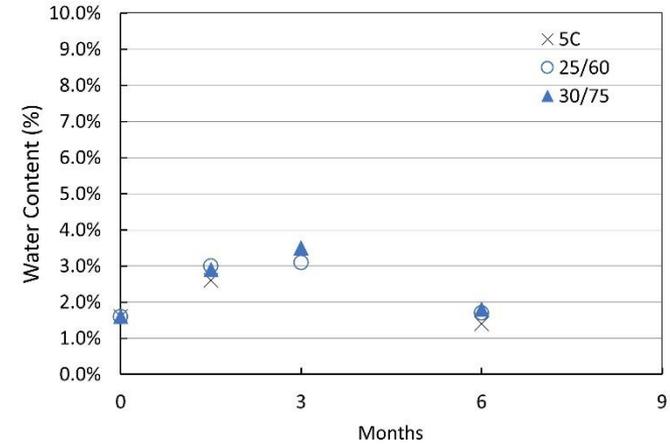
Stability was monitored on crimped FD vials

Water content and assay were consistent for 6 months under

- 5 °C
- 25 °C 60% RH
- 30 °C 75% RH

No impurities was increasing

Redispersion time remained at 30s with vortex



# Application of ANP formulation

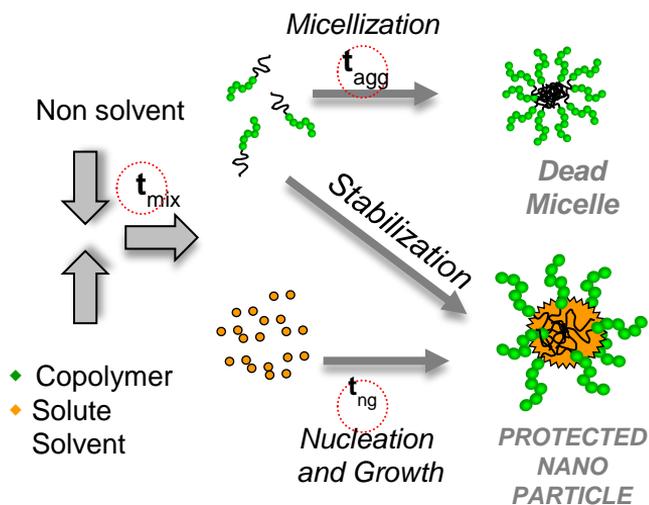
- **Extremely low solubility**
- **High melting point (not suitable for hot melt extrusion)**
- **High pill burden**



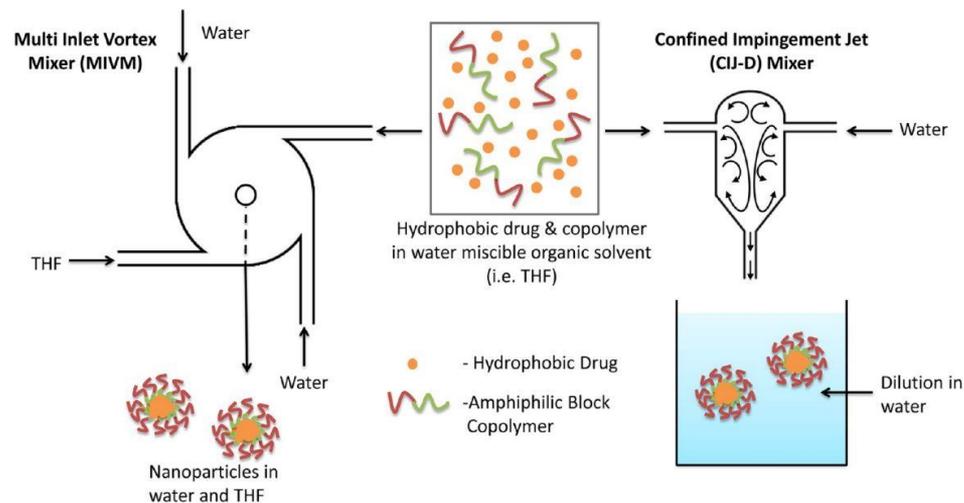
# Formation of nanoparticles – solvent anti-solvent precipitation

- Controlled mixing of API solution with antisolvent with at high *Reynold's Number*
- Supersaturation leads to precipitation and encapsulation of API in polymer/surfactant

## Mechanism of NanoPrecipitation



## Design of mixing devices



### Flash Nanoprecipitation: Particle Structure and Stability

Pustulka and Macosko et al., *Mol. Pharmaceutics* 2013, 10, 4367–4377

### Controlling drug nanoparticle formation by rapid precipitation

Suzanne M. D'Addio, Robert K. Prud'homme, *Adv. Drug Deliver. Rev.* 2011, 63 417-426